Filling-up and Overflow in a Tank Example

NOTE: This is <u>a typical, general type problem</u>, for which no specific prerequisites are necessary. An intelligent man may solve it without using calculus, see the last methods (c) and (d) on page 3. This is a simple problem solved as <u>an example to show how several different methods may be used in general.</u>



Problem: A tank providing water to a pump is shown in Figure. Water <u>enters</u> the tank trough a 1-in diameter supply pipe at a <u>constant</u> mass flow rate of 6.8 lb/s (m_{in}), and exits to the pump through a 1-in diameter (d_e) pipe. The diameter of the tank is 18 in. (d_T), and the top of the 2-in diameter (d_{of}) overflow pipe is 2 ft (z_{top}) from the base of the tank. The velocity V_e, in ft/s, of the water <u>exiting</u> to the pump varies with the height z of the water surface from the bottom, in ft, according to: $V_e(z)=8.16z^{1/2}$. Determine the time (T), in seconds, for the control volume enclosing the initially empty tank to reach steady state (when overflow begins, $z=z_{top}$). At steady state, what is the mass flow rate, in lb/s, that water spills out through the overflow pipe?

Setting up the problem:

Given: d _e	$=\frac{1}{12}$	$d_{T} := \frac{18}{12}$	$d_{of} := \frac{2}{12}$	z _{top} := 2	$V_{e}(z) := 8.16 \cdot \sqrt{z}$, also:	ρ := 62.34
$A_e := d_e^2 \cdot \frac{\pi}{4}$	Ae	$= 5.454 \cdot 10^{-3}$	A _T :=	$\left(d_{T}^{2} - d_{of}^{2}\right)$	$\frac{\pi}{4}$ A _T = 1.74	5	exit-pipe and tank-base areas, respectively

<u>Conservation of mass</u>: "small" mass (**dm**) and height (**dz**) increases for a small time period (**dt**), see the darker shaded area on the Figure above:

 $m_{in} := 6.8 \dots$ constant in-flow mass rate $m_e(z) := \rho \cdot A_e \cdot V_e(z)$

 $dm = \rho \cdot A_T \cdot dz = (m_{in} - m_e(z)) \cdot dt$

 $D = \frac{dz}{dt} = \frac{\left(m_{\text{ in}} - m_{\text{ e}}(z)\right)}{\left(\rho \cdot A_{\text{ T}}\right)} = C_1 - C_2 \sqrt{z} \text{ where: } C_1 := \frac{m_{\text{ in}}}{\rho \cdot A_{\text{ T}}} \quad C_1 = 0.0625 \quad C_2 := \frac{A_e}{A_{\text{ T}}} \cdot 8.16 \quad C_2 = 0.0255$

a) Solving the above differential equation for "dt" by separation of variables and integrating:

...MathCAD numerical integration
$$z_{top} = 2$$

 $T_a := \int_{0}^{e^z top} \frac{1}{(C_1 - C_2 \cdot \sqrt{z})} dz$ $T_a = 54.47$

...MathCAD symbolic/analitic integration

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$$\frac{1}{\left(C_{1} - C_{2} \cdot \sqrt{z}\right)} dz \Rightarrow 54.4789751206557729$$

...the solution, i.e. the time needed to fill-up the empty tank till its overflow level.

NOTE: Different subscripts may be used for the same physical variables to indicate the corresponding method, for example (T_a) or (T_b) or (T_l) , or to differentiate results obtained using different methods.

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$$I(z) := \frac{-\ln(C_1^2 - C_2^2 \cdot z)}{C_2^2} \cdot C_1 - 2 \cdot \frac{\sqrt{z}}{C_2} + 2 \cdot \frac{C_1^2}{\left[C_2 \cdot \left(\sqrt{-C_2^2} \cdot \sqrt{C_1^2}\right)\right]} \cdot \operatorname{atan}\left(\sqrt{-C_2^2} \cdot \frac{\sqrt{z}}{\sqrt{C_1^2}}\right)$$

...the analytical indefinite integral of the above expression

Also, $T_I := I(z_{top}) - I(0)$ $T_I = 54.479$...the solution, i.e. the time needed to fill-up the empty tank till its overflow level.

As we often see, the **analytical integration is usually lengthy** <u>or impossible</u>, so **we**, **engineers**, **resort to numerical solutions**. That is no longer difficult, if we utilize available (and now powerful and inexpensive) PC computational hardware and application software, see below.

b) Solving the above differential equation (see page 1) by *Runge-Kutta* numerical method (with *rkfixed*(), a built-in MathCAD function - have to be used if the separation of variables is not possible):

 $z_0 := 0 \qquad D(t,z) := C_1 - C_2 \cdot \sqrt{z_0} \qquad \qquad \text{...initial value and derivative of the function } \mathbf{z}(t) \\ t_0 := 0 \qquad t_L := 100 \qquad N_1 := 500 \qquad \qquad \text{...initial- and end-values of the independent variable } \mathbf{t} \\ \text{and number of points over that range}$

 $Z := \text{rkfixed}(z, t_0, t_L, N_1 - 1, D) \quad N := \text{rows}(Z) \quad N = 500 \quad M := \text{cols}(Z) \quad M = 2 \quad (Z^{<1>})_{N-1} = 3.001256$

$$t_b := Z^{<0>} z_b$$

 $= Z^{\leq 1>}$...the solution of the above differential equation (see page 1) over the range $t_0 < t < t_{L}$



The Runge-Kutta method (see also MathCAD Help, or press F1 key while cursor is on "*rkfixed*" function) is a very effective to solve any first-order ordinary differential equation (ODE), or a system of the first order ODEs (thus higher-order DE) for a given initial value(s). However, to evaluate the independent variable, t in this case, for a given value of dependent variable $z=z_{top}=2$, we have to "look" in the table of solution values, or on the diagram, or to try different t-values until we obtain the given z=2 value, in this case. Luckily, MathCAD has the built-in "Given-Find" solver to do almost any iterative "search" for us, see next (This procedure may be also used to solve the so-called boundary-value problems using the initial value problem methods):

Define the solution as function of
$$t_{top}$$
: $Z_b(t_{top}) := rkfixed(z, t_0, t_{top}, N-1, D)$ $z_{Top}(t_{top}) := (Z_b(t_{top})^{<1>})_{N-1}$

Guess: $t_{top} = 40$...and use the "Given-Find" solver below to find new $T_b = t_{top}$ to satisfy the required condition

Given

 $z_{Top}(t_{top})=2$... given condition

 $T_b := Find(t_{top})$ $T_b = 54.479$...the solution, i.e. the time needed to fill-up the empty tank till its overflow level.

Check the z-value for the calculated T_b value, i.e. that the condition above is $z_{Top}(T_b) = 2$ satisfied:

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C) Solving the above differential equation (see page 1) by dividing the function z-range in N divisions and using the finite difference approximation (this is a "common sense" method):





d) Solving the above problem (see page 1) by approximating variable exit flow rate with a constant flow rate based on average water height during the fill-up

<u>NOTE:</u> This is a "common sense" simplified method which may or may not be appropriate for a given case. <u>Be very cautious when using it.</u>

$$z_{avg} := \frac{0 + z_{top}}{2}$$
 $m_{e_av} := m_e(z_{avg})$ $T_d := \frac{\rho \cdot A_T \cdot z_{top}}{m_{in} - m_{e_av}}$ $T_d = 54.057$ $\frac{T_d}{T_I} = 99.2$ %

The T_d compares pretty well with the above results (T_a , T_l , T_b , T_c), since the relation between z and t is "almost" linear (see above diagram). However, we have to be very cautious in general when using such approximations.

<u>The steady-state solution (at z = z_{top} = 2 = constant)</u>:

 $m_{in} = 6.8$... in-flow mass rate $m_{e_top} := m_e(z_{top})$ $m_{e_top} = 3.924$... exit-flow mass rate $m_{overflow} := m_{in} - m_{e_top}$ $m_{overflow} = 2.876$... over-flow mass rate(c)1998 by Prof. M. Kostic

http://www.ceet.niu.edu/faculty/kostic/